



UNIVERSITÀ DEGLI STUDI  
DI MODENA E REGGIO EMILIA  
**DIPARTIMENTO DI INGEGNERIA "ENZO FERRARI"**  
Via Vignolesse, 905 – 41126 MODENA (Italy)

# **ADVANCEMENTS IN UNDERSTANDING WATER-MIST SYSTEMS: FROM SPRAY CHARACTERIZATION TO REAL-SCALE APPLICATIONS**

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# Agenda and Problem Statement



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## Task 1 - Spray Characterization

- What are the discharge characteristics of water-mist sprays issued by commercial nozzles?
- What physical parameters are to be investigated to quantitatively assess their performance?
- What spray-related mechanisms are of significant interest in determining suppression?

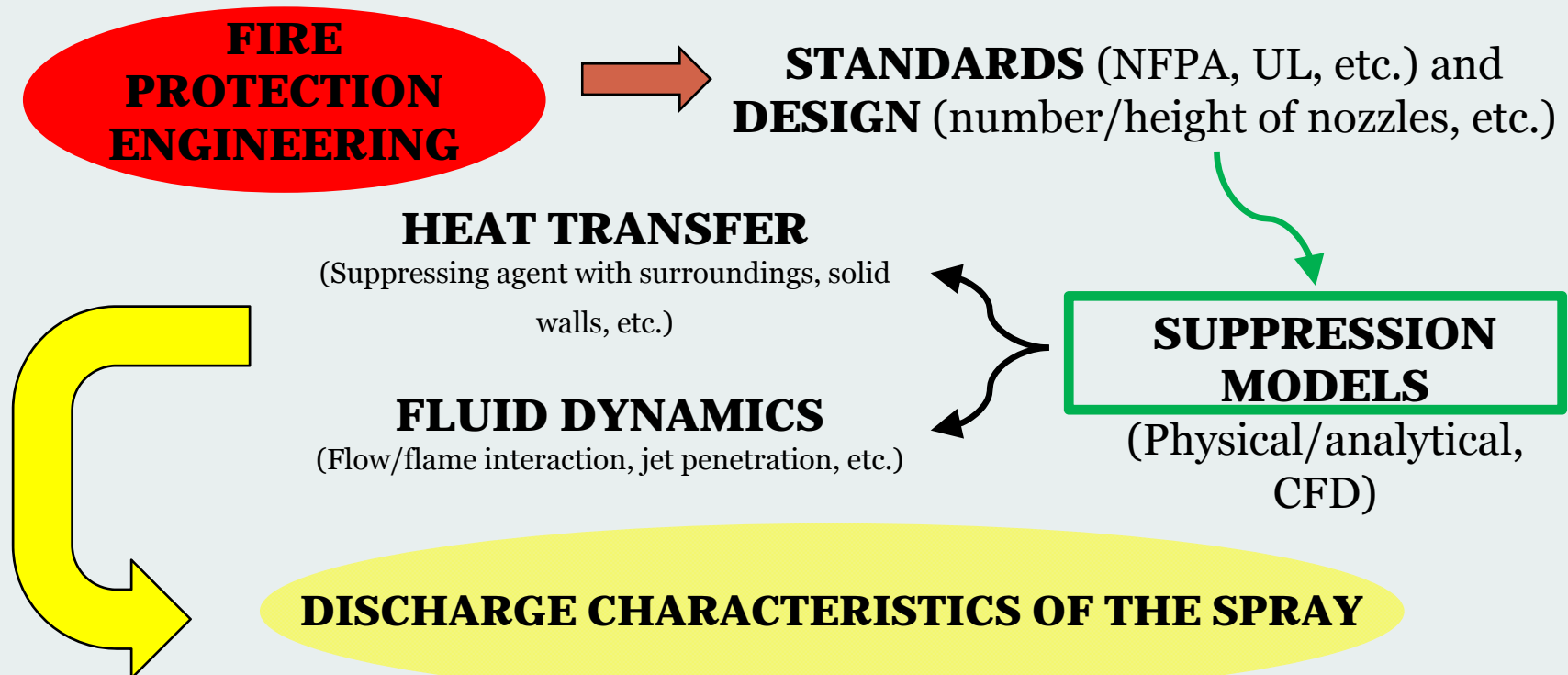
## Task 2 - Suppression in Full-Scale Scenarios

- How does the spray actually perform against a real-scale severe fire case?
- What parameters are to be measured to quantitatively evaluate suppression performance?
- How is suppression performance influenced by the introduction of additives to water?



# Task 1 - Motivation

TO PROVIDE A DETAILED CHARACTERIZATION OF WATER-MIST SPRAYS  
IN TERMS OF **DROP-SIZE DISTRIBUTION** AND **SPATIAL DISPERSION**



# Background and Recent Advancements



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## Main References:

- **Wang et al.**, Exp. Fluids 33 (2002) 587-593. Low pressure (2-8 bar), PIV + Digital-Image Processing. Main results: drop size and velocity distribution at 1 m distance from the orifice. Other: breakup length.
- **Paulsen Husted et al.**, Fire Saf. J. 44 (2009) 1030-1045. High pressure (100 bar), hollow- and full-cone nozzles, PIV and PDA. Main results: comparison of these techniques, drop size and axial velocity in the initial region of the spray.
- **Santangelo**, Exp. Therm. Fluid Sci. 34 (2010) 1353-1366. High pressure (60-80 bar), full-cone nozzle, *Malvern Spraytec*, PIV, mechanical patternator. Main results: drop-size and flux distribution at 1 m distance from the orifice, velocity field and spray-cone angle in the initial region of the spray. Other: breakup length.
- **Santangelo et al.**, Proc. IMECE2011 6 (2011) 1167-1174. High pressure (80 bar), hollow-cone nozzle, *Malvern Spraytec*, PIV, mechanical patternator. Main results: drop-size axial trend from the orifice throughout 1-m distance, initial velocity, parametric analysis.

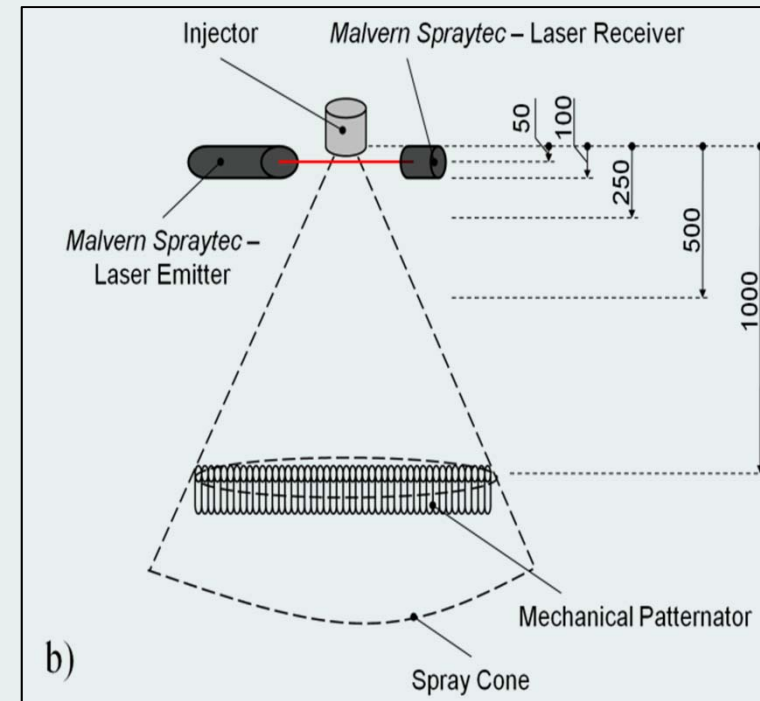
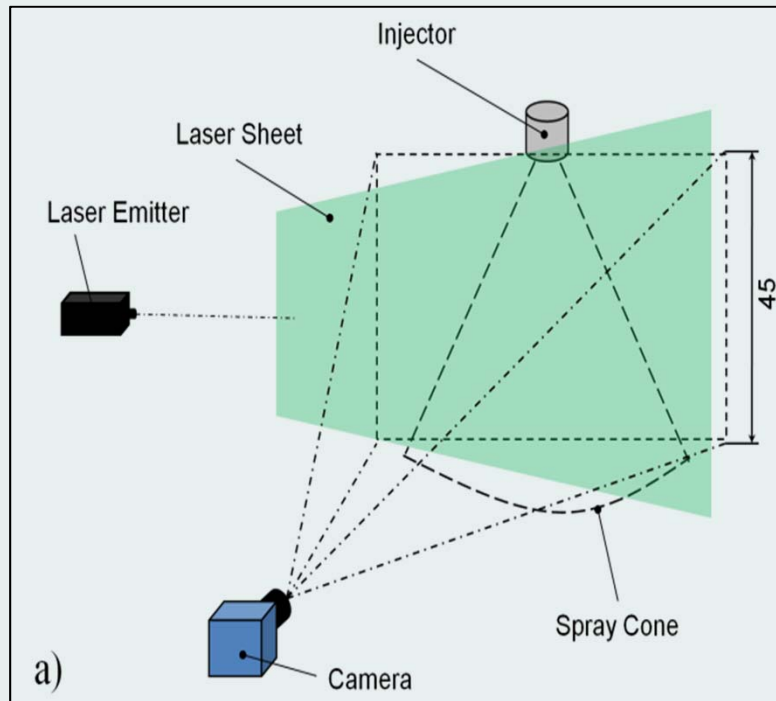
## Recent Developments:

- Drop-size axial evolution: potential **coalescence** and **secondary atomization**.
- **Initial velocity** and **cone angle** for hollow-cone water-mist sprays.
- **Parametric analysis** comparing different orifices (flow number, outlet diameter).

# Experimental Setup for Spray Analysis



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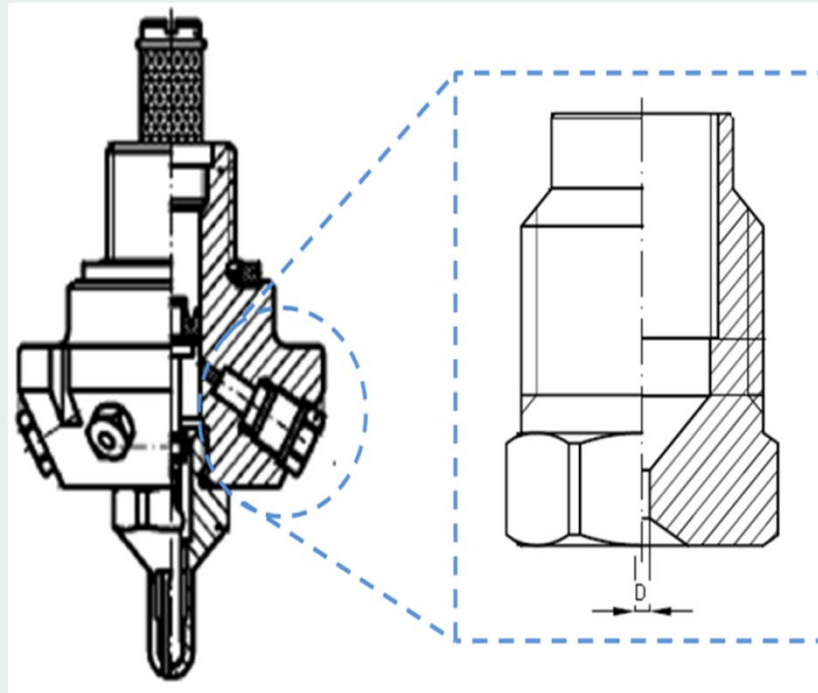
Sketch of the experimental apparatus:

- a) PIV setup (velocity field and spray-cone angle);
  - b) *Malvern Spraytec* and mechanical patternator (droplet size).
- All dimensions are in mm.

# Employed Nozzles and Injectors



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*CJX* series by *Bettati Antincendio S.r.l.* (pressure-swirl atomizers, hollow-cone sprays), here operated at 80 bar (pressure right upstream the injector)

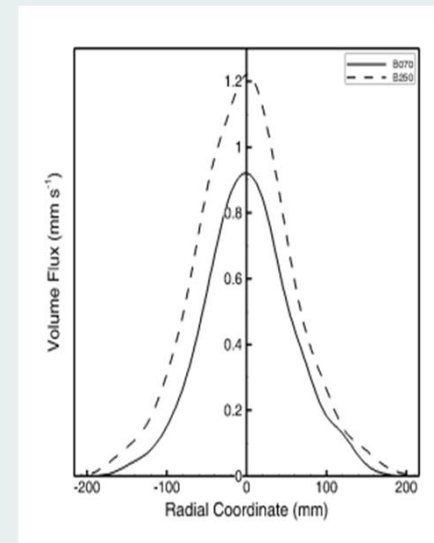
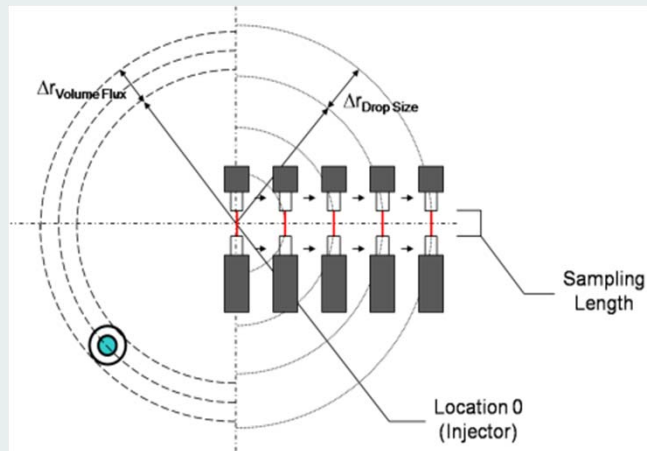
Injector	Orifice Diameter (mm)	Flow Number (lpm bar <sup>-0.5</sup> )
<i>B070</i>	0.49	0.1167
<i>B250</i>	1.14	0.4167

# Drop-Size Experimental Procedure



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- Radial symmetry of the spray is assumed as a simplifying hypothesis.
- At 5, 10, 25 and 50 cm distance from the injector outlet, the drop-size distribution consists of the crude *Malvern Spraytec* results along a generic diameter.
- At 1 m distance from the injector outlet, a flux-based weighting procedure is employed to reconstruct the overall drop-size distribution, thus overtaking the biasing effect due to the mismatch between the geometric shape of *Malvern Spraytec* sampling volume and the spray cross section.
- Volume flux is yielded by patteration tests.



Equation to reconstruct the volume fraction pertaining to the  $i$ th drop size over all the  $j$  measurement locations:

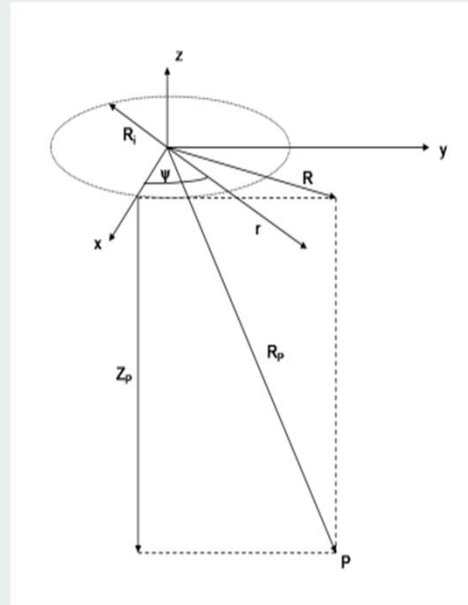
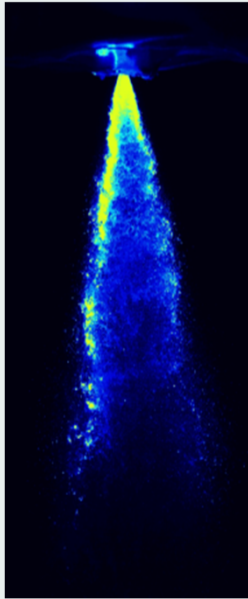
$$V_i'' = \sum_{j=1}^N q_j'' \cdot \frac{1}{\rho_L} \cdot \frac{\Delta r}{R} \cdot VF_{i,j}$$



# PIV Analysis: Parameters and Procedure



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- The PIV apparatus features a 30 mJ pulsed-Nd:YAG laser (by *Dantec Dynamics*), a thermo-electrically cooled CCD camera (14 bit, 4 Mpixels) and a post-processing software (by *LaVision*).
- Measurements have been taken at 4 Hz frequency, with a time interval of 5  $\mu$ s between two exposures of the same pair.

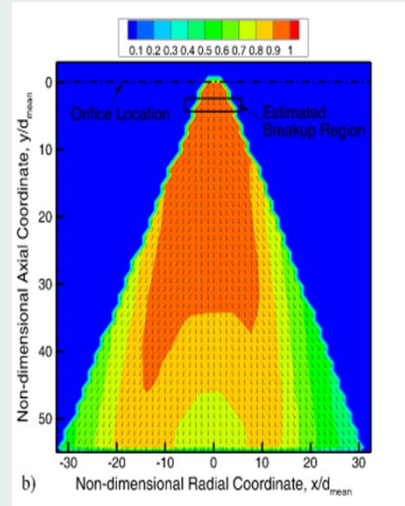
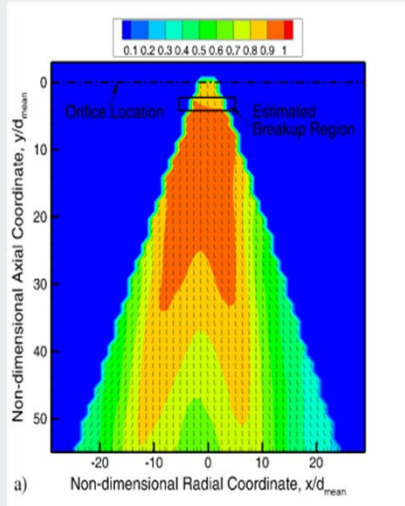
- No seeding has been added: droplets constitute tracking particles themselves.
- Only axial and radial velocity components have been considered, because the tangential tends to collapse onto this latter within few millimeters downstream the outlet.
- LSV (Laser Speckle Velocimetry) has been employed to process images in the highly-saturated region (axially stretching over about 5 mm from the orifice).
- Results upstream the breakup location are to be considered as unreliable (continuum flow).
- The velocity field has been reconstructed over a set of 300 images.



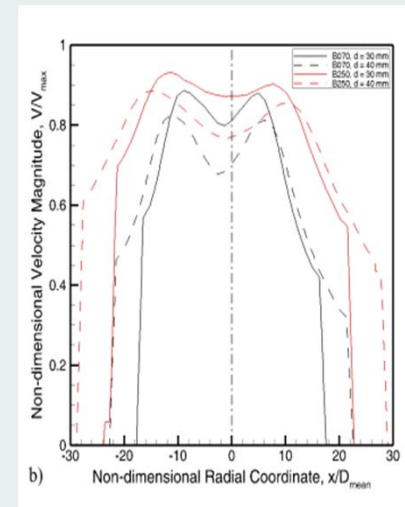
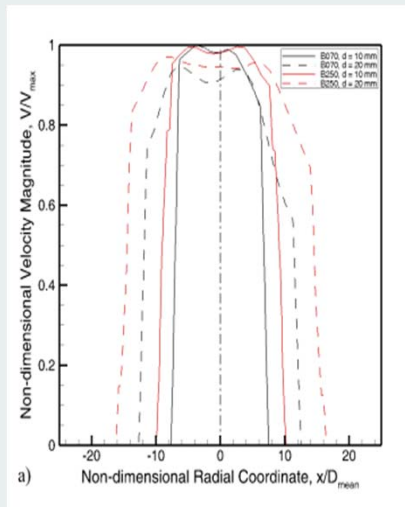
# PIV Results: Velocity Maps and Profiles



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Map of velocity magnitude for  
a)  $B070$  ( $V_{max} \approx 101 \text{ m s}^{-1}$ ) and  
b)  $B250$  ( $V_{max} \approx 85 \text{ m s}^{-1}$ ) injectors

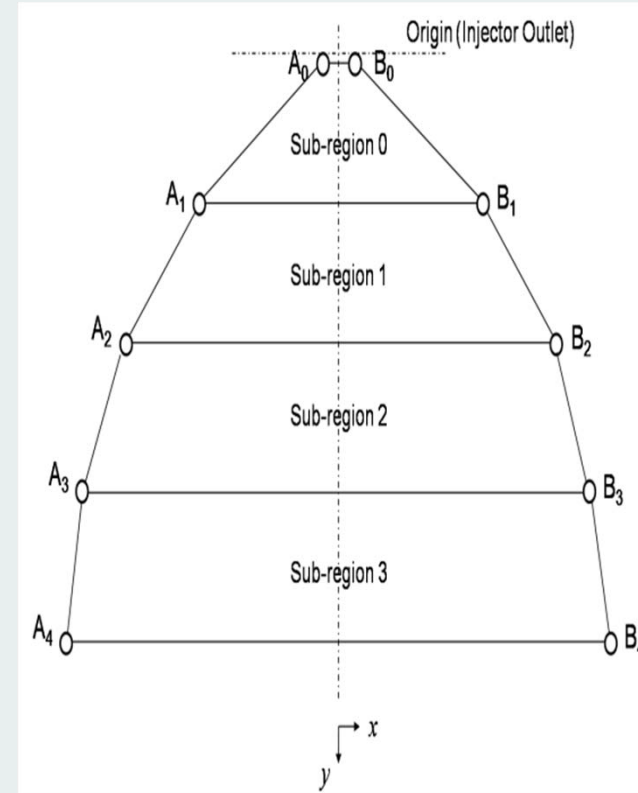
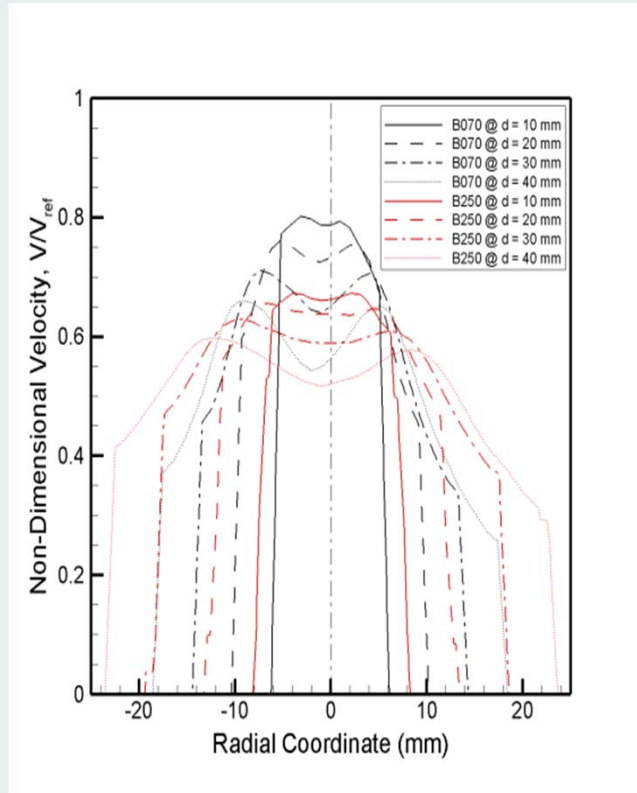


Radial velocity profiles in the region  
a) close to the orifice (10-20 mm)  
and  
b) far from the orifice (30-40 mm).

# PIV Results: Evaluation of Spray-Cone Angle



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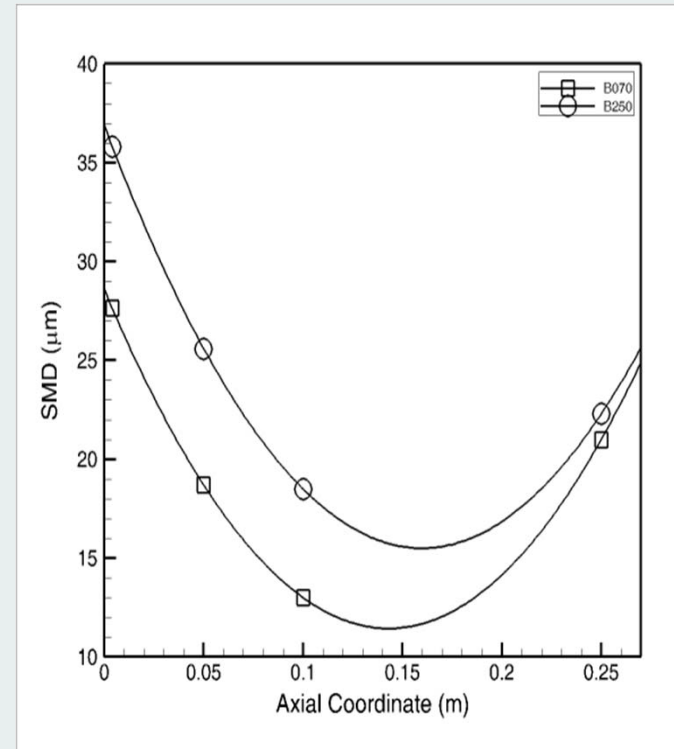
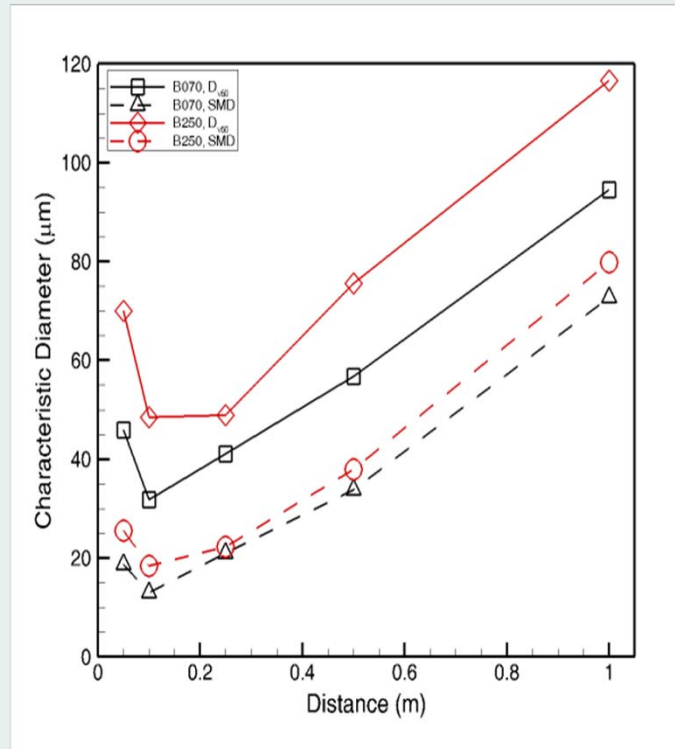
The cone boundary is identified by radial locations ( $x$ ) where velocity magnitude turns into 0

$$\theta = \arctan \frac{|x(A_{k+1}) - x(A_k)|}{|y(A_{k+1}) - y(A_k)|}, \quad k = 0, 1, 2, 3$$

# Drop-Size Experimental Results



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- Coalescence phenomena appear to govern droplet size after secondary atomization has occurred (about 15 cm downstream the outlet).
- The same qualitative drop-size trend is shown by both the injectors, even though larger diameters are generated by the bigger orifice.
- An attempt to extrapolate SMD at the supposed breakup location (4 mm downstream the outlet) has been made through a simple 3<sup>rd</sup>-degree polynomial curve.

# Physical Modeling for Initial Velocity



The classic inviscid model developed by Giffen and Muraszew (Atomization of Liquid Fuels, Chapman & Hall, London, UK, 1953) for pressure-swirl atomizers inspired some theoretical analysis to predict velocity and spray-cone angle.

$$\sin\theta_{th} = \frac{(\pi/2)C_D}{K(1+X^{0.5})}$$

$$K^2 = \frac{\pi^2(1-X)^3}{32X^2}$$

$$C_D = \left[ \frac{(1-X)^3}{1+X} \right]^{0.5} \quad C_D = \frac{FN}{A_o} \left( \frac{\rho_L}{2} \right)^{0.5}$$

$$V_{th} = \frac{Q}{X \cdot A_o}$$

Injector	Theoretical half cone angle, $\theta_{th}$ (°)	Experimental half cone angle, $\theta_{th}$ (°)	Cone-angle relative error	Theoretical velocity, $V_{th}$ (m s <sup>-1</sup> )	Experimental velocity, $V$ (m s <sup>-1</sup> )	Velocity relative error
B070	16.66	26.90	38.07%	108.63	101.40	7.13%
B250	30.61	35.40	13.52%	90.23	85.39	5.66%

# Physical Modeling for Droplet Size



The very first physical parameter to be investigated is sheet thickness, which is

$$t = \frac{d_o \cdot (1 - X^{0.5})}{2}$$

Rizk and Lefebvre (J. Propul. Power 1 (1985) 193-199) found that initial SMD is proportional to  $t^{0.39}$  in pressure-swirl atomizers: this relation was mainly connected to fuel sprays, but results to be correct for water-mist too.

Lefebvre (Atom. Spray Technol. 3 (1987) 37-51) discusses the characteristic diameter as constituted by two contributions:

- **First stage:** disruptive hydro- and aerodynamic forces,  $f((Re \cdot We^{0.5})^{-c})$ ;
- **Second stage:** velocity gradients,  $f(We^{-g})$ .

Wang and Lefebvre (J. Propul. Power 3 (1987) 11-18) provide an expression for SMD under certain ranges for dynamic viscosity and surface tension:

$$SMD = 4.52 \cdot \left( \frac{\sigma \mu_L^2}{\rho_A \Delta P_L^2} \right)^{0.25} (t \cdot \cos \theta)^{0.25} + 0.39 \cdot \left( \frac{\sigma \rho_L}{\rho_A \Delta P_L} \right)^{0.25} (t \cdot \cos \theta)^{0.75}$$

Injector	Theoretical sheet thickness, $t$ (mm)	Extrapolated SMD (mm)	$SMD/t^{0.39}$	Modeled SMD	SMD relative error
B070	149.78	27.64	3.92	28.14	1.80%
B250	244.77	35.83	4.19	37.34	4.21%

## Task 2 – Main References and Motivation

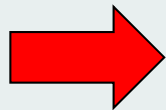


### References:

- Experimental and numerical studies on flow-flame interaction of water-mist sprays in simple heptane pool fires (P.E. Santangelo et al., Proc. 14<sup>th</sup> Int. Heat Transf. Conf. 5 (2010) 571-580);
- Experimental tests of water-mist discharge against high-rise-storage fires, within a highly equipped large-scale facility (P.E. Santangelo and P. Tartarini, Appl. Therm. Eng. 45-46 (2012) 99-107; P.E. Santangelo and P. Tartarini, Proc. 12<sup>th</sup> Int. Conf. Multiph. Flow Ind. Plants (2011) paper V.4).

### Objectives:

- Challenging water-mist fire-suppression performance in a large-scale and highly hazardous scenario;
- Comparing suppression capabilities with and without a commercially available additive.



**Water-mist tests in a High-Hazard Storage facility (UNI EN 12845); additive F-500 by *Hazard Control Technologies Inc.***

# Parameters of Suppression Performance



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- The fire should be **spatially controlled**, preventing the surrounding materials (i.e., the target shelf) from being burnt;
- The higher temperatures within the domain should be **limited under conservative values** to preserve the structural configuration of the building (i.e., the test chamber);
- The temperatures at eye level should be **kept as low as possible** to allow the best conditions for fire fighters;
- The fire spread within the involved commodities (i.e.: in the main shelves) should **be vertically and horizontally limited** as much as possible to optimize the rate of damages.

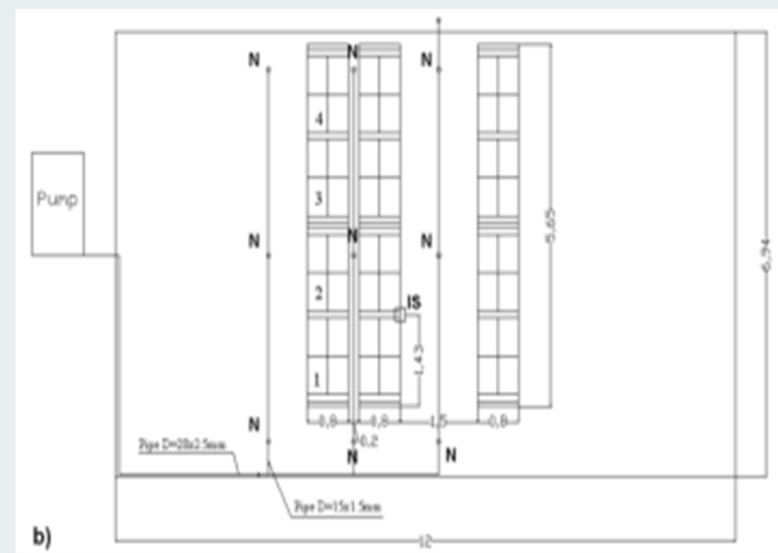


# Experimental Setup



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- **Test chamber:** Prefabricated iron box, base area  $\sim 83 \text{ m}^2$  ( $12 \text{ m} \times 6.94 \text{ m} \times 8 \text{ m}$ );
- **Storage structure:** Iron beams, 3 shelves ( $5.65 \text{ m} \times 0.8 \text{ m} \times 6.89 \text{ m}$  each), 8 storage levels;
- **Nozzle:** CJX 1140 B1SG by *Bettati Antincendio S.r.l.*, 7 injectors (total flow number =  $1.4 \text{ l min}^{-1} \text{ bar}^{-0.5}$ ); 9 nozzles located at the ceiling above the ignition-involved shelves;
- **Electric pump:** Maximum static head = 130 bar, operative pressure at the nozzle inlet = 100 bar.



**Technical sketch of the experimental facility: a) view from side; b) view from above**

# Combustible Materials

## Commodities (*EUR Standard Plastic Commodities*):

- wooden pallets,
- cardboard boxes,
- plastic glasses.

	Wooden pallets	Cardboard boxes	Polystyrene glasses
Main shelves	64	256	30 720
Target shelf	32	128	15 360
Total amount	96	384	46 080
Total mass (kg)	2 400	691.20	138.24

Material	Lower Heat Value (MJ kg <sup>-1</sup> ), <i>H</i>	Combustion Efficacy, $\phi$	Limiting Coefficient, $\psi$
Wood	19	0.8	1
Cardboard	17	0.8	1
Polystyrene	40	1	1

**NOMINAL FIRE LOAD:**

$$q_f = \frac{\sum_{i=1}^N m_i \cdot H_i \cdot \phi_i \cdot \psi_i}{A} = 617.33 \text{ MJ m}^{-2}$$

# Experimental Facility – Photos



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# Experimental Measurements and Procedure



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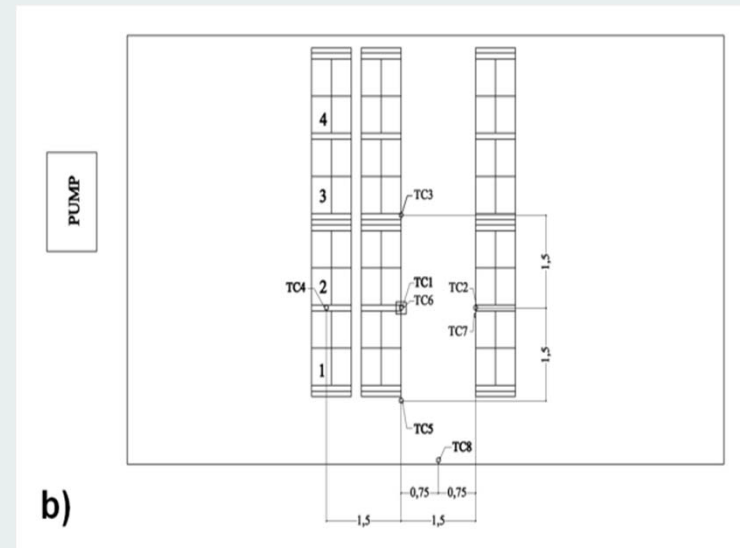
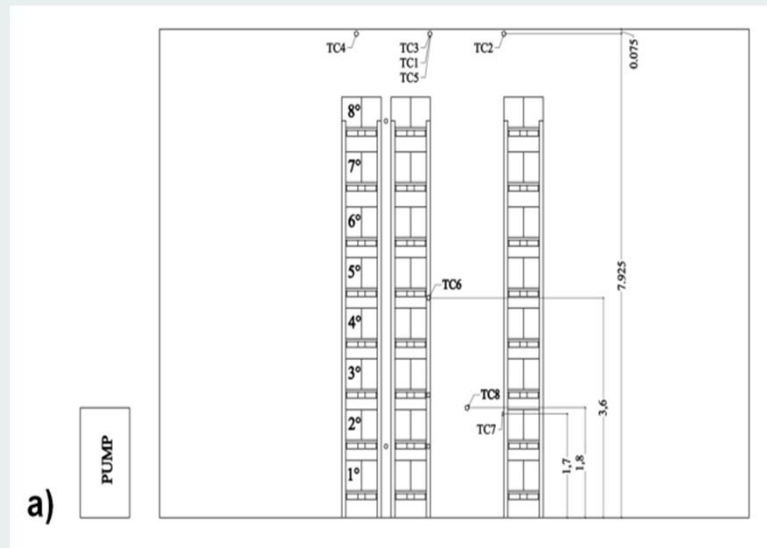
- **Thermocouples:** K type, diameter = 0.5 mm. 5 (TC1-TC5) placed between the ceiling and the nozzle height (hot gas temperature), 1 (TC6) placed at the flame axis 3.6 m distant from ignition source, 1 (TC7) placed at the target shelf, 1 (TC8) placed at eye-level height in between the shelves;
- **Thermal-response wires:** Activation temperature = 88 °C, all wires placed along the ignition-involved shelves at 1.1, 1.9 and 6.5 m from the floor;
- **Ignition source:** Heptane pool fire (120 ml), placed below the ignition-involved shelves;
- **Discharge:** 30 min; Test 1 - sole water, Test 2 - water/F-500 (2% volumetric concentration); if temperature at the ceiling = 350 °C, the test is interrupted (manual extinction for building preservation; failed suppression);
- **Water-mist activation:** both thermal-response-wire and temperature based.

Report From the Sensors	Discharge-Activation Time (s)
Alarm from 3 thermal-response wires within 60 s after ignition	60
Alarm from 2 thermal-response wires within 90 s after ignition	90
No/1 alarm from thermal-response wires within 120 s after ignition	120
Ceiling temperature = 300 °C	Immediate

# Thermocouple Assembly



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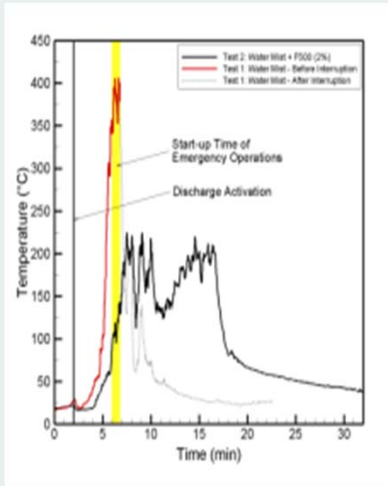
## Locations

- **Ceiling Height:** 5 thermocouples (TC1-5) to measure hot-gas temperature;
- **Main Shelves:** 1 thermocouple (TC6) at the axis of the heptane pool fire to measure flame temperature;
- **Target Shelf:** 1 thermocouple (TC7) to measure the potential involvement of the target shelf;
- **Eye Level:** 1 thermocouple (TC8) to measure the environmental conditions for fire fighters.

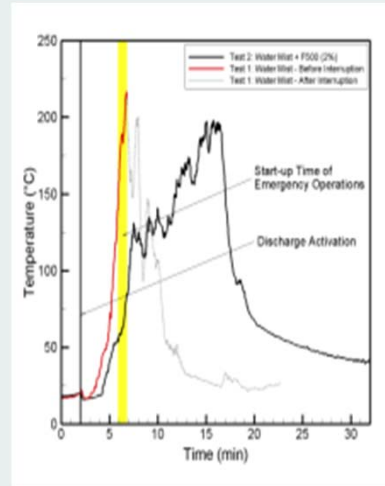
# Temperature Profiles (TC1-TC6)



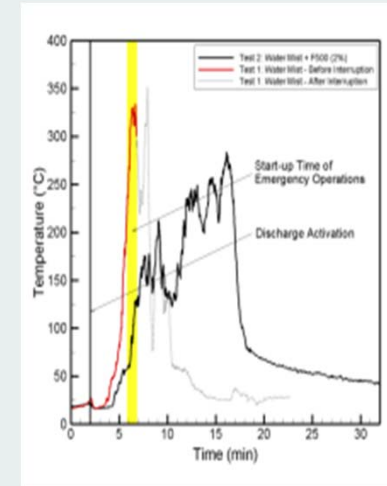
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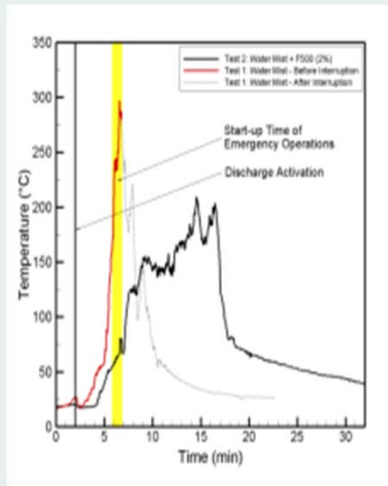
TC1 - Ceiling



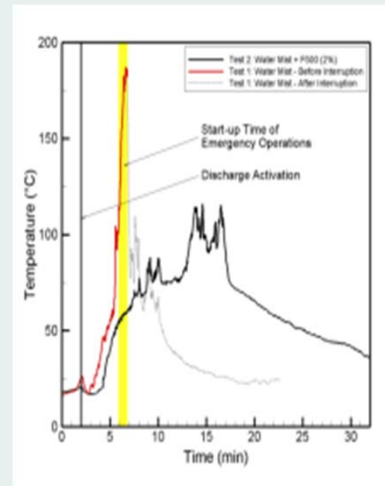
TC2 - Ceiling



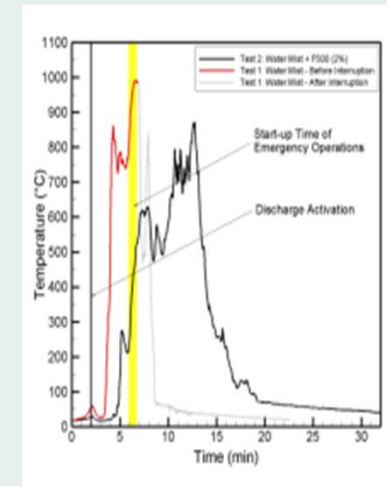
TC3 - Ceiling



TC4 - Ceiling



TC5 - Ceiling

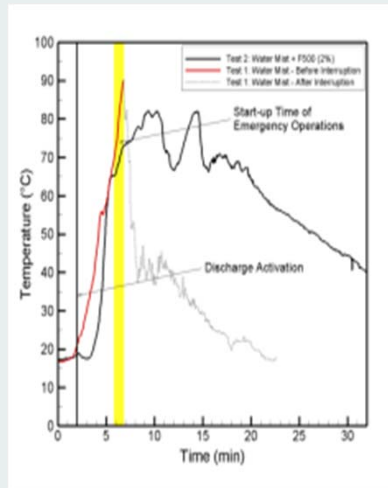


TC6 - Flame axis

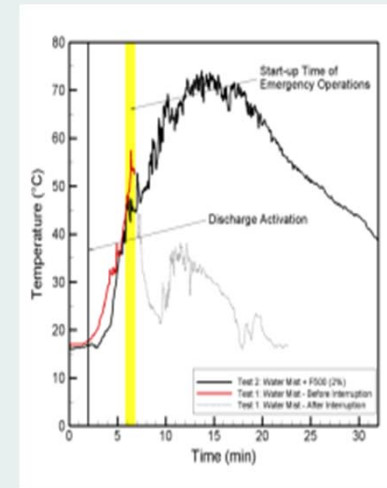
# Temperature Profiles (TC7, TC8 and details)



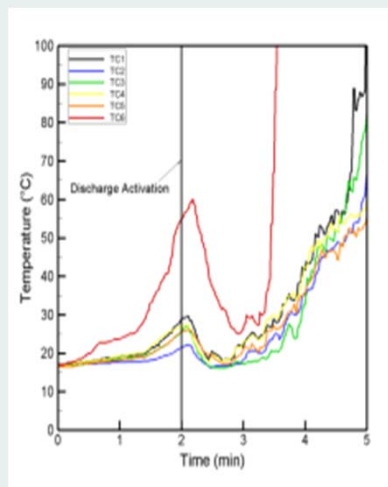
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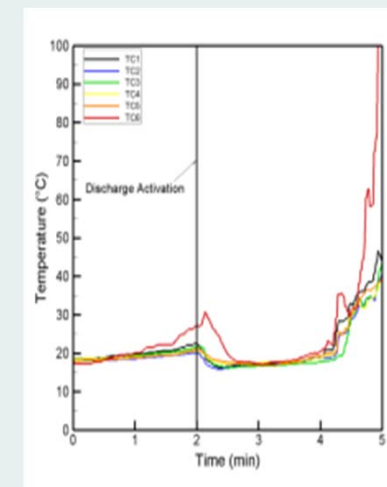
TC7 - Target shelf



TC8 - Eye-level height, hallway



TC1-TC6 after ignition (sole-water flow)



TC1-TC6 after ignition (water/F500 flow)



# Additional Outcomes



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## Mass-loss evaluation:

- No mass-loss actual measurement was carried out, since the main scope was to evaluate thermal control and because the size of the involved experiments;
- Following a post-fire damage evaluation, 4 pallets (base) and 6 storage levels (height) in the main shelves were involved in the fire spread for both the tests;
- As a conservative assumption, 25% and 37.5% of the combustible materials were burnt in Test 1 (sole water) and Test 2 (water/F-500) respectively;
- As an additional assumption, burning in Test 1 is assumed to stop at the end of emergency operations ( $0.16 t_{Discharge}$ ), while burning in Test 2 is assumed to stop at the end of the discharge;
- Considering a free-burn time of 120 s (as in both tests), the **average burning rate in Test 1 is 3.15 higher** than in **Test 2**.

## How does the presence of an additive affect drop size?

- Relative viscosity (to water) appears to be the main governing parameter in determining droplet size in water/surfactants (retardants) flows;
- According to F-500 declared components, its relative viscosity seems to be quite high (1.6-7.7);
- This case seems to be similar to agricultural water/drift retardant sprays;
- Drop size is assumed to **increase** by **35%** ( $D_{v50}$ ) with respect to the sole-water flow.

# Conclusions



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- An experimental investigation was conducted to investigate velocity field, spray-cone angle drop-size axial evolution in water-mist sprays generated by two hollow-cone nozzles, employing laser-based diagnostics.
- The velocity field shows the same qualitative characteristics for both the injectors, while the cone angle is wider for larger orifices.
- Drop-size trends show that secondary atomization is the governing phenomenon until a minimum is reached; then, coalescence tends to increase droplet size.
- Drop-size trends are qualitatively very similar, but larger orifices tend to generate bigger droplet size on an average basis.
- Some predictive relations for pressure-swirl atomizers have been successfully validated for the water-mist case, as a result of non-viscous modeling.
- A water-mist system operating at high pressure was challenged in suppressing a fire within a high-hazard scenario; sole-water and water/additive flow were employed;
- Thermal transients was considered as the main parameter to determine suppression performance, together with post-fire damage evaluation and a temperature safety threshold;
- The sole water has been proved to provide ineffective action, even enhancing the temperature rise (turbulent effect on fire); on the other hand, the water/F500 flow yielded to successful thermal control and fire suppression;
- Fire spread was mainly vertical over both the tests (reduced temperature rise at the target shelf); eye-level temperature was lower than 80 °C over both the tests, thus allowing safe fire-fighters' operations.

# Future Work



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- Coupled velocity and drop-size measurements are to be pursued, employing shadowgraphy as one of the possible techniques.
- A more accurate patternation system should be designed to collect the smaller floating particles, thus implying an indirect evaluation of the evaporated share of the whole spray.
- Statistic analyses on turbulence can be conducted on PIV images, thus evaluating air entrainment within the spray.
- Modeling air entrainment in hollow-cone sprays still needs to be accomplished.
- Additional full-scale tests under downsized configurations should be performed to carry out a scaling approach on the involved physical phenomena;
- Numerical simulations of the fire scenario through CFD codes should be attempted to evaluate their predictability in terms of temperature profile and fire spread.



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# Thanks for your kind attention.

## Questions?

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